

LEWICE 2.2 Capabilities and Validation

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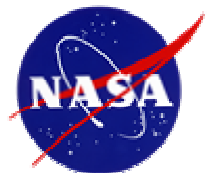
Aug. 22, 2002

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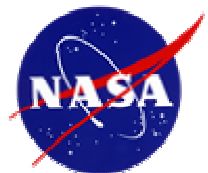
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Outline

- **Background**
- **Bleed Air Capabilities**
- **External Review**
- **Heat Transfer Correlations**
- **Validation Tasks**



LEWICE

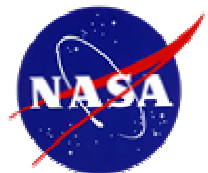
- **Flow Solver**
 - Use potential panel code to determine flow field about clean surface
- **Droplet Trajectories**
 - Calculate water droplet trajectories from some upstream location until impact on the surface or until body is bypassed
- **Water Collection**
 - Determine water droplet impact location pattern between impingement limits
- **Heat Transfer**
 - Perform quasi-steady analysis of control volume mass and energy balance in time stepping routine
- **Ice Growth**
 - Density correlations used to convert ice growth mass into volume
- **Iterate**
 - With new ice shape, iterate entire routine

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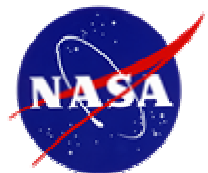
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LEWICE/Thermal

Thermal Ice Protection System Simulation

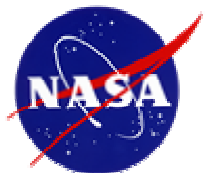
- **Approach**
 - Used LEWICE model for flow field and trajectories
 - 2D unsteady heat transfer model
- **Features**
 - Composite body structure
 - Individual heater sequence with different power to each heater
 - Gaps between heaters
 - Predicts ice accretion, shedding, melting, and refreezing
 - Water runback on surface using the LEWICE model



ANTICE

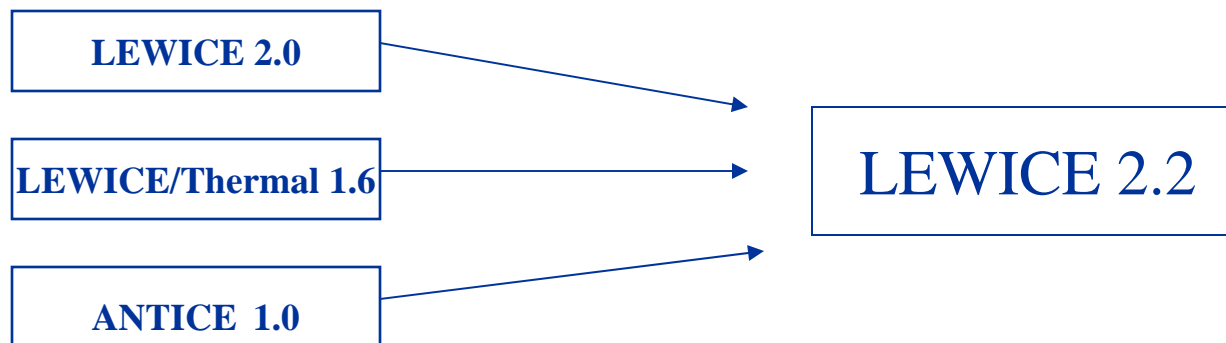
Thermal Anti-Icing Simulation

- **Approach**
 - Flow and trajectory solutions required from other sources
 - 2D steady heat transfer model
- **Features**
 - Composite body
 - Multi-zone electro-thermal heaters with different power densities
 - Gaps between heaters
 - Hot gas anti-icing system (streamwise gas flow)
 - Specified surface heat flux distribution
 - Surface water runback and surface wetness factor (rivulet model)
 - Partial and full evaporation, and freezing



LEWICE 2.2

- **Combines features of LEWICE, LEWICE/Thermal and ANTICE**
 - Multi-time step
 - De-icing or Anti-icing
 - Electrothermal or hot air
 - Uses results from other sources
- **Added features**
 - Optimized heater sequencing
 - Multiple boundary conditions for bleed air analysis

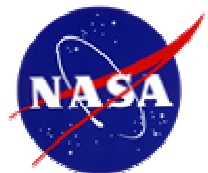


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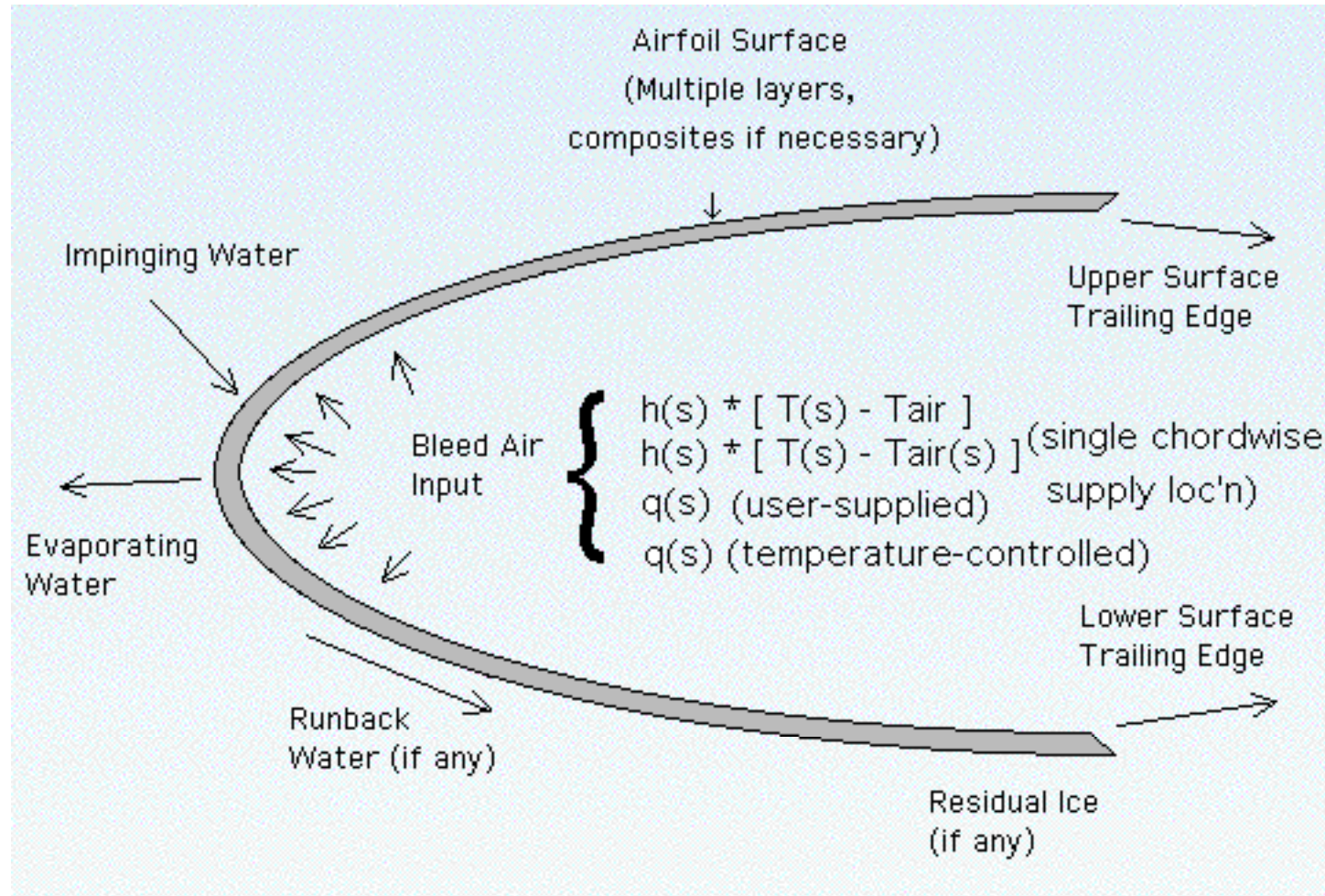
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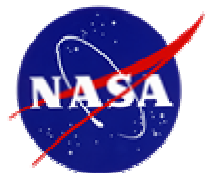


Bleed Air Capabilities



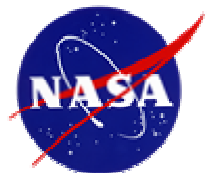
Bleed Air Boundary Conditions

- **Convective HTC user-supplied**
 - Constant bulk temperature in bleed air (multiple supply locations)
 - Variable bulk temperature in bleed air (user-supplied input location)
- **Inner surface heat flux user-supplied**
- **Inner surface heat flux controlled by temperature**
- **All should be capable of modeling piccolo tube design**
 - Multiple methods provided for user convenience
- **Requires separate method to translate design criteria (hole size, spacing, mass flow rate, etc.) into required input**

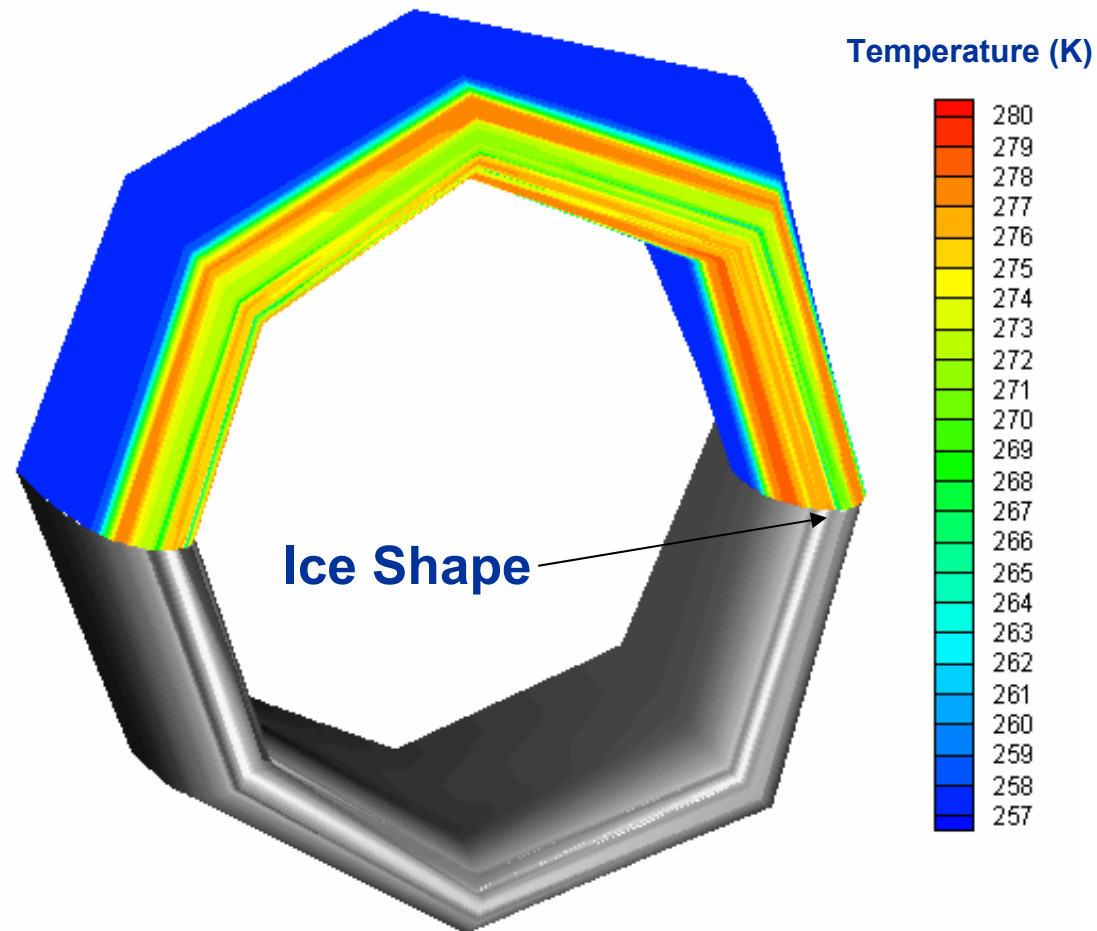


Bleed Air Test Case

- Half-Model Symmetric Engine Inlet
- LEWICE 3D Example Case
- 5 Thermal Runs Obtained on Each 2D Streamline
- Bleed Air Flow Rate Reduced To Obtain Runback for Illustration
- $V = 150$ kts, $LWC = 0.2$ g/m³, $MVD = 20$ μ m, $T = 0^{\circ}$ F, $t = 3$ min



Bleed Air Test Case

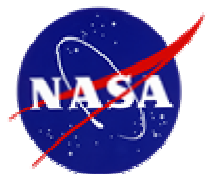


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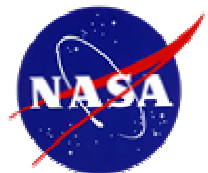
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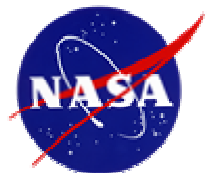
External Reviews

- **Academic Review**
 - Software verification
 - Grid sensitivity
 - Time-step sensitivity
- **Industry Review**
 - Applicability to piccolo tube systems
 - Usability of software
 - Accuracy of results
 - 18%-30% lower than experiment



Review Recommendations

- **Change data inputs**
 - Inputs should be d , T , P , z_n , c_n rather than h_{tc} or q arrays
- **Include surface temperature array as input**
 - Useful for calibration
- **Develop experimental database**
- **Use a fixed reference point for wrap distance**
- **Implement a fixed transition point for b.l.**
- **Fix two program errors “bugs”**
 - Dual heat flux b.c.
 - Large anisotropic ratios



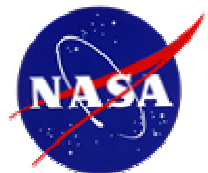
Changes Due to Review

- Included all suggested user options
- Fixed program errors
- Added correlations for piccolo heat transfer

$$\overline{Nu} = C * \text{Pr}^{1/3} * \text{Re}^a * \left(\frac{z_n}{d}\right)^b * \left(\frac{c_n}{d}\right)^e$$

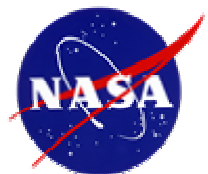
- Variation in powers from literature
- $C = 0.453$, $a = 0.691$, $b = -0.22$, $e = -0.38$ (Tawfek) $6 \leq z_n/d \leq 58$
- $C = 0.251$, $a = 0.68$, $b = 0.15$, $e = -0.38$ (Gau & Chung) $2 \leq z_n/d \leq 8$
- $C = 0.394$, $a = 0.68$, $b = -0.32$, $e = -0.38$ (Gau & Chung) $8 \leq z_n/d \leq 16$

$$\overline{Nu} = \text{Re}^{0.76} * \left[\frac{24 - \left| \frac{z_n}{d} - 7.75 \right|}{533 + 44 * \left(\frac{c_n}{d} \right)^{1.394}} \right] \quad (\text{Goldstein et. al.})$$



Electrothermal Validation

- Two week entry in 1996
- NACA0012 airfoil
- Electrothermal heater designed by Cox & Co.
- 100+ cases
 - 12 tunnel conditions
 - De-icing and anti-icing runs for each condition



Validation Test Model

- **NACA0012 airfoil, 36" chord**

Mounted vertically

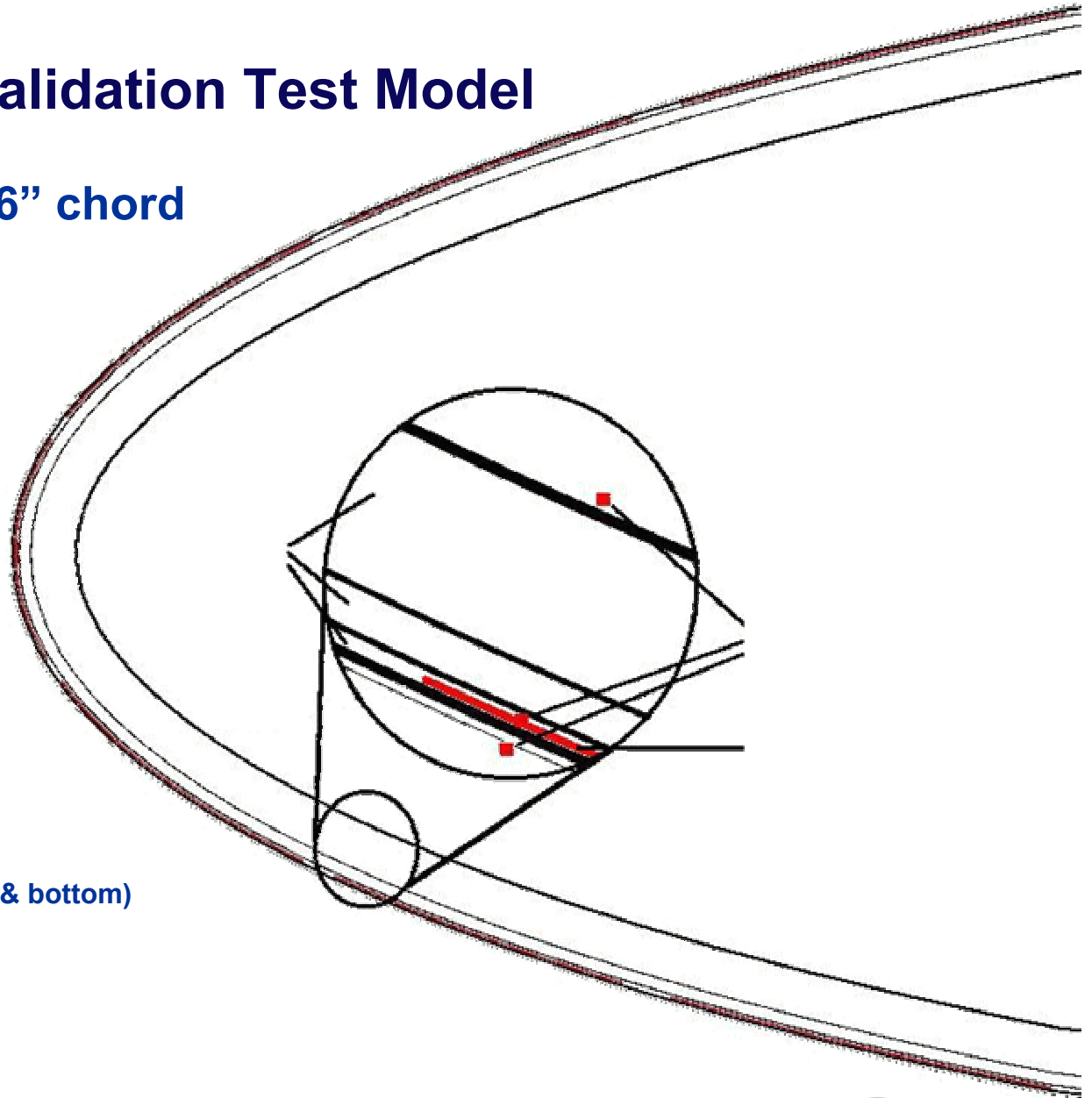
- **7 Heaters**

- **3 Operative Modes**

- Running Wet
- Evaporative
- De-icing

- **Data Acquisition**

- Photos
- Video
 - Standard VCR
 - BetaCam
 - InfraRed
- 42 Thermocouples
 - 3 per heater location
 - 2 sets of heaters (top & bottom)

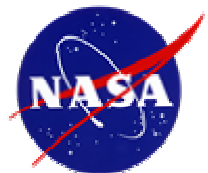


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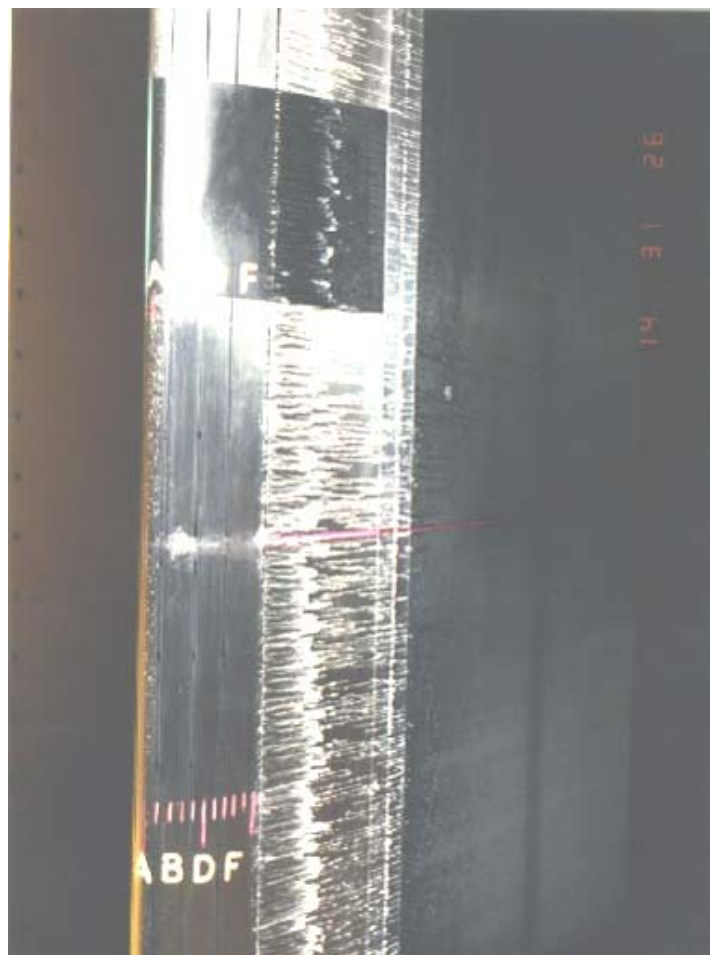
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Run22 Anti-Icing Case

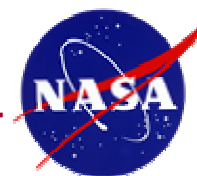


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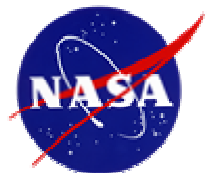
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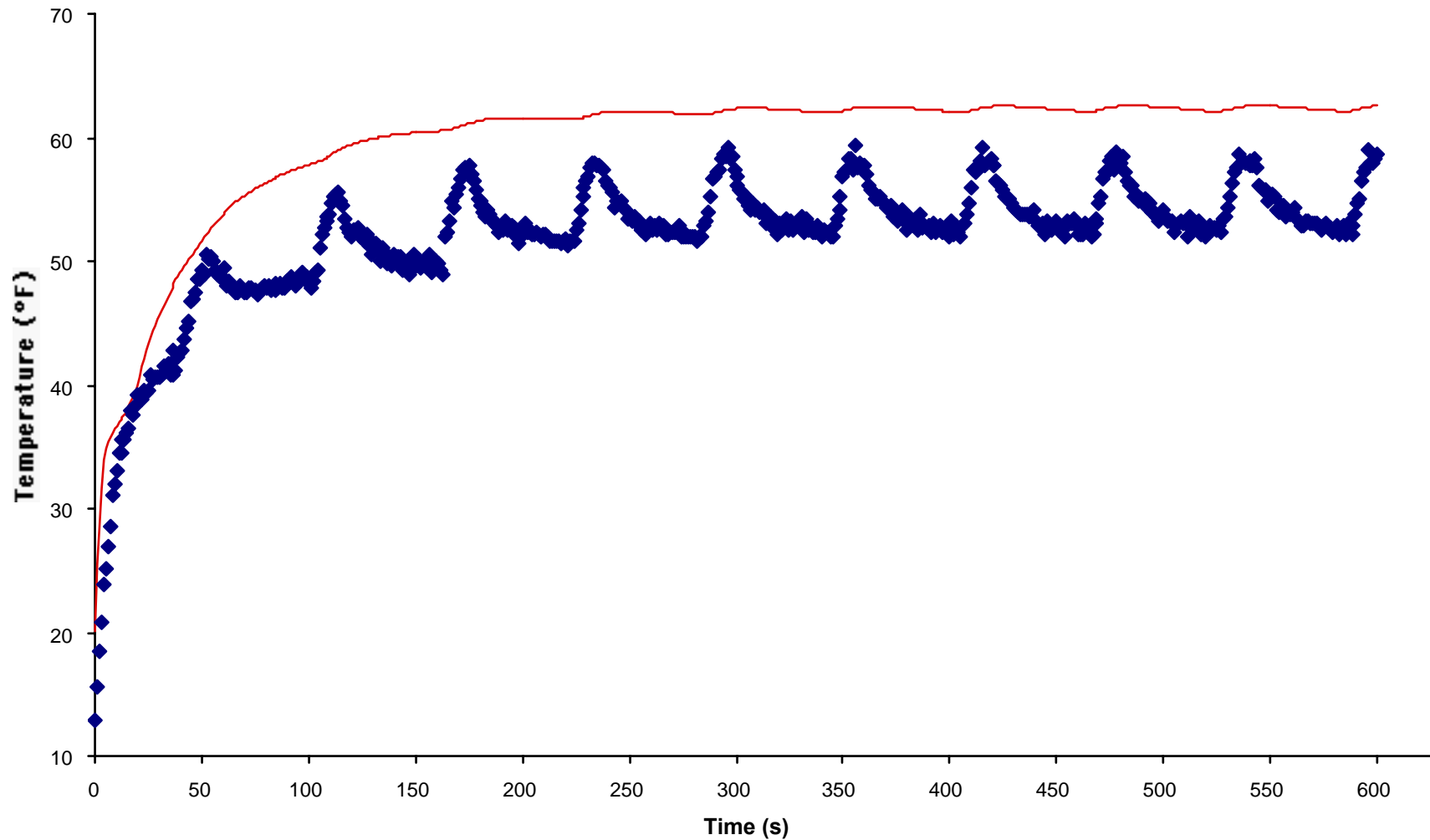
Electrothermal Validation Tasks

- **Coordinate experimental data**
- **Run cases**
- **Parametric studies**
 - Power variations
 - Material property/thickness variations
 - Grid density (more points/time steps)
- **Compare data**
 - Percent error
 - Absolute error
 - Comparison plots
- **Validation report**



Sample Electrothermal Validation (Laminar)

Run 17 Top, Section A: Heater Temperature



◆ Section A: Heater Temperature (Experimental) [°F]

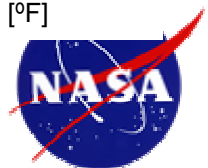
— Section A: Heater Temperature (LEWICE) [°F]

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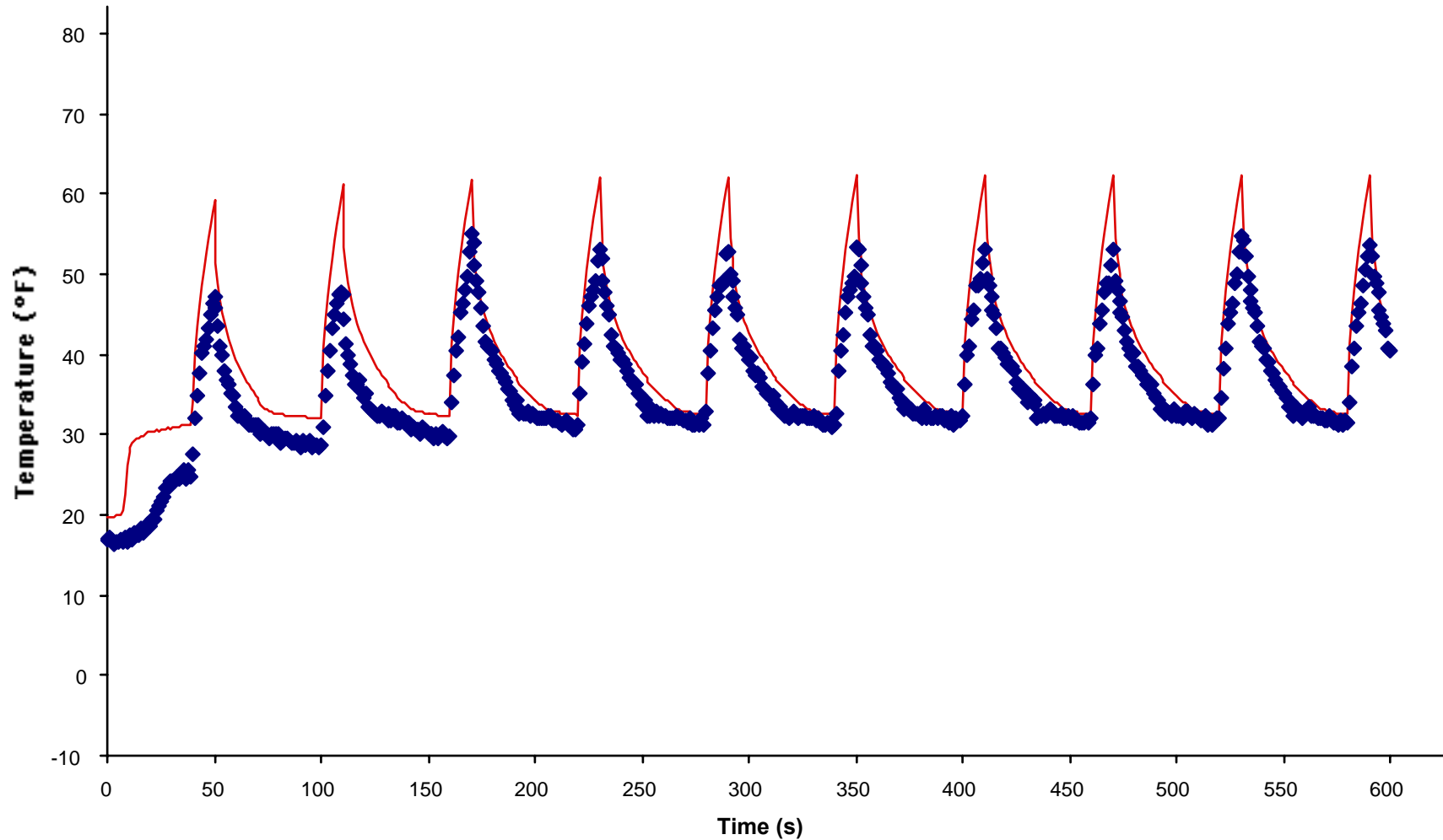
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Sample Electrothermal Validation (Laminar)

Run 17 Top, Section B: Heater Temperature



◆ Section B: Heater Temperature (Experimental) [°F]

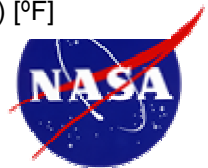
— Section B: Heater Temperature (LEWICE) [°F]

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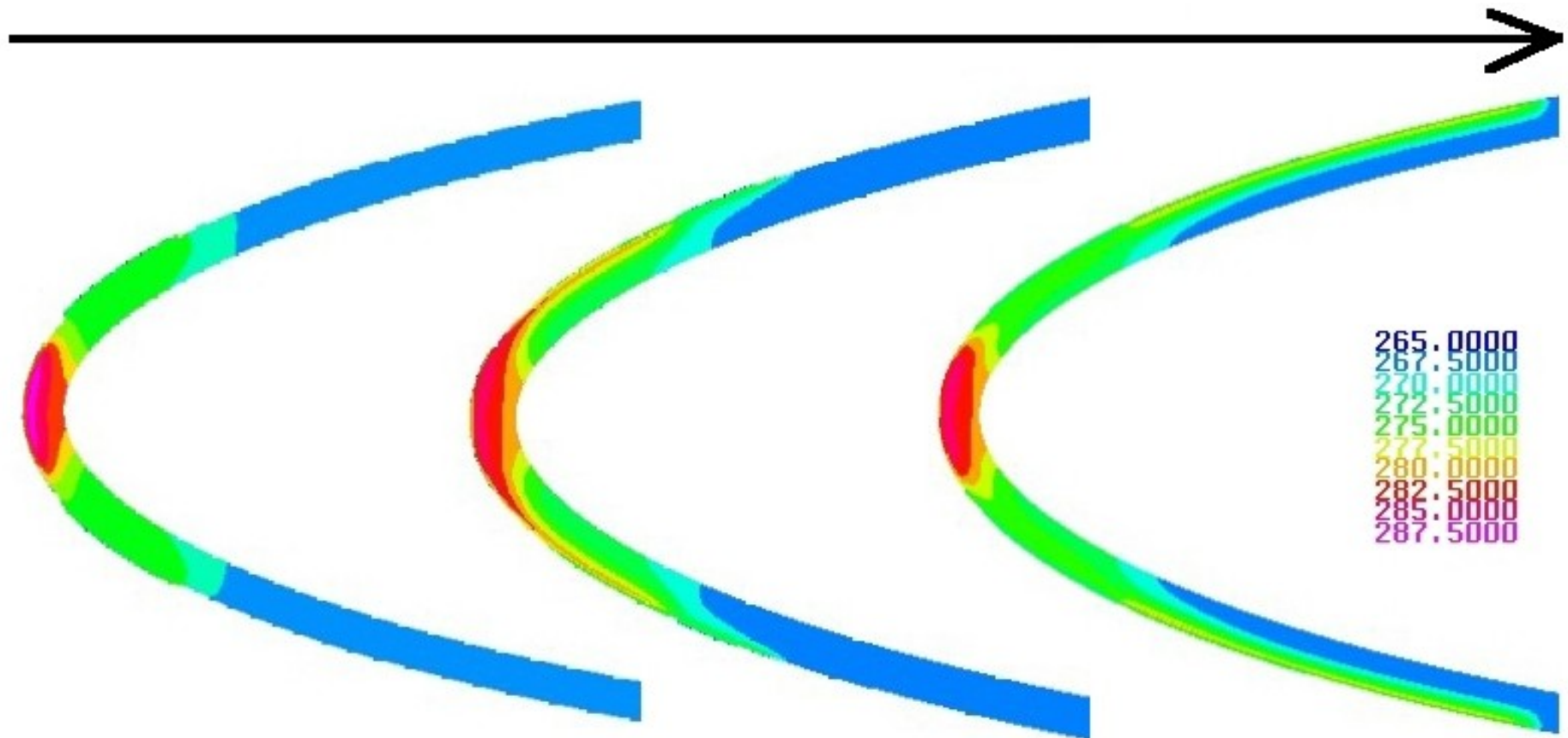
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Typical Temperature Progression

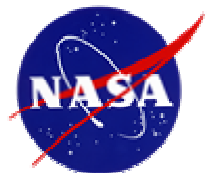


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Variability of Results

$$\text{absolute difference} = |T_{\text{exp}} - T_{LEW}|$$

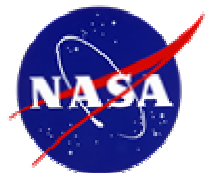
$$\text{percent difference} = |T_{\text{exp}} - T_{LEW}| / (T_{\text{exp max}} - T_{\text{exp min}})$$

	% Error	Estimated Difference	Avg. % Difference	Avg. Absolute Difference	Avg. % Difference	Avg. Absolute Difference
Mode	Experimental	Experimental	Expert User	Expert User	Untrained User	Untrained User
De-Icing	9%	3 °F	18%	6 °F	35%	11 °F
Anti-Icing	22%	8 °F	45%	16 °F	89%	31 °F
Overall	13%	6 °F	26%	13 °F	51%	25 °F



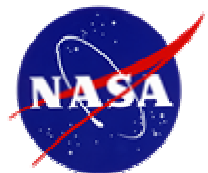
Quantitative Results

	Laminar, Sectional Shed		Laminar, Nodal Shed		Turbulent, Sectional Shed	
	Avg. % Difference	Avg. Absolute Difference	Avg. % Difference	Avg. Absolute Difference	Avg. % Difference	Avg. Absolute Difference
Overall Deicing	8.6°F	25.7%	9.2°F	29.6%	8.8°F	27.2%
20°F Cases	6.5°F	26.3%	7.3°F	29.6%	5.9°F	22.4%
0°F Cases	11.9°F	24.5%	12.2°F	29.6%	13.2°F	29.0%
Evap. Anti- Icing	35°F	22.7%	55°F	35.6%	88.6°F	56.0%
Running Wet	22.2°F	38.0%	25.6°F	44.2%	33.4°F	53.9%



Ice Shape Results

- **Preliminary Validation of Ice Shape Characteristics**
 - All cases ran using automated process (not validated)
- **Insignificant Difference for Most Cases**
 - All average parameters within 2% of LEWICE 2.0 results
 - Majority of parameters < 1% difference from LEWICE 2.0



Conclusions

- **Bleed Air and Electrothermal Capabilities Available**
- **Electrothermal Validation Performed**
 - Reasonable (25%) accuracy for deicing or anti-icing applications
 - Code results can be calibrated if desired
- **Additional Data Needed**
 - Bleed air anti-icers
 - Investigate evaporative physics to improve accuracy

